

Vanadium Production in Europe

Carbon-neutral, zero-waste vanadium recovery from slag

Dr David Robinson

International Circular Hydrometallurgy Symposium (ICHS) | September 2024

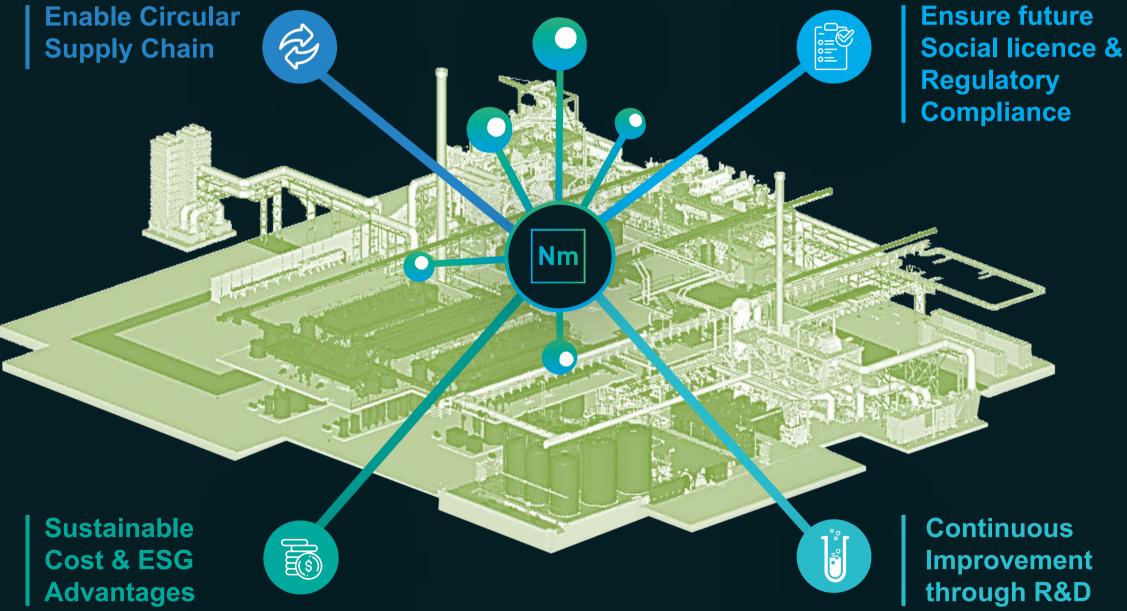
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Corporate

Focus (What We Do)

Commercialising our portfolio of sustainable process technologies to recycle and recover critical materials from high-value waste streams





- Primobius JV is building Mercedes-Benz a 2,500tpa integrated spoke and hub pilot plant
- Product readiness for ~21,000tpa commercial plants expected 2H2025
- Lithium Chemical and Vanadium Recovery technologies approaching Industrial Partner Validation stage of development

Corporate

Lithium-ion Battery (LiB) Recycling

Primobius (50:50 Joint-Venture with SMS Group)

Off-spec and used battery recycling to produce metal salts for battery production

- Demonstration Plant near Hilchenbach, Germany
- Battery shredder and feed material beneficiation
- Cu, Mn, Co, Ni and Li recovery and refining (hydromet circuit)
- Battery quality metal salts for return to • battery manufacture
- Commercial plant under contract (Mercedes)
- Visit:

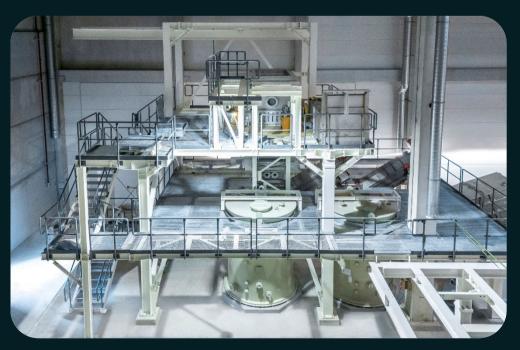
www.neometals.com.au/businessunits/core-divisions/lib/









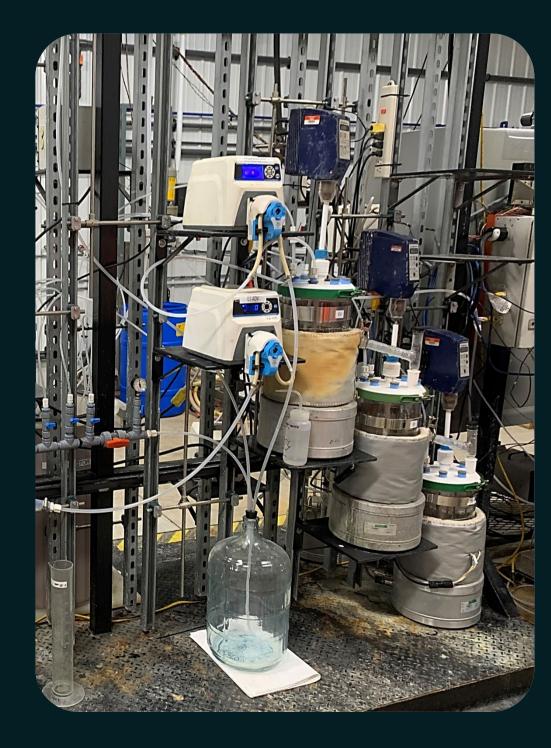


Lithium Chemicals

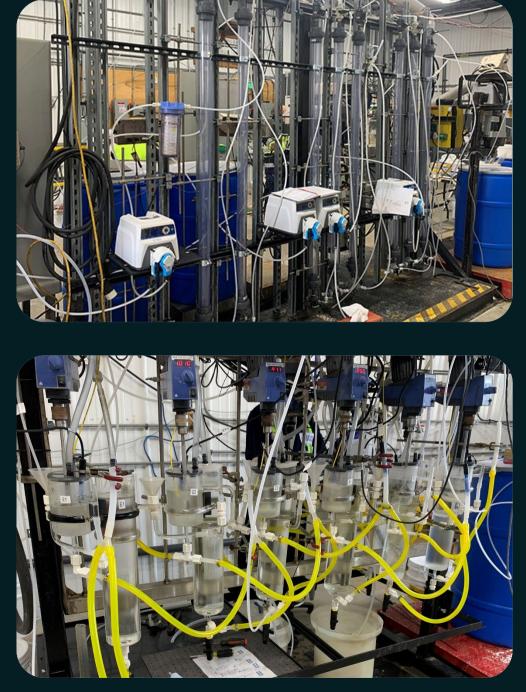
ELi[™] the direct production of lithium hydroxide Reduced processing and lower cost production of LHM

- Processing lithium brine concentrates or spodumene leach solutions
- Patented purification of lithium chloride solution and electrolysis to convert directly to lithium hydroxide solution
- Bench and pilot demonstration, including 1,000-hour electrolysis demonstration of technology.
- Visit:

<u>www.neometals.com.au/business-</u> <u>units/core-divisions/lithium-</u> <u>chemicals/</u>









Novana Oy

Hydrometallurgical recovery of vanadium from steel slag

- Background on SSAB and the vanadium rich steel slag
- Flowsheet Development
- Commercial Aspects
- Life Cycle Analysis and Project status
- Visit: <u>www.neometals.com.au/business-</u> <u>units/core-divisions/vanadium-recovery</u>











Vanadium Recovery

Vanadium Recovery Process Technology

100% Neometals



What is Vanadium?

Vanadium is a chemical element which appears as a hard, silvery-grey, malleable transition metal.

- Light first row transition metal with +2, +3, +4 and +5 oxidation states.
- Supply and demand dominated by China.
- Consumption dominated by China and ferrovanadium (Rebar) production.
- Future Vanadium Flow **Batteries**



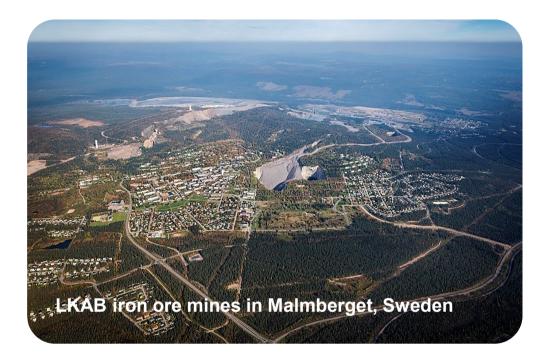




Where does the Story Begin?

From the ore to the smelter feed...

- LKAB iron ore mines in Malmberget, Sweden.
- The ore contains vanadium.
- LKAB iron pellets from Malmberget contain approximately 0.24%
 V₂O₅ (vanadium pentoxide).
- Pellets are sold worldwide, including to SSAB.











From the Ore to Steel Products

- LKAB iron ore pellets are one of the main ingredients in steel produced at the SSAB steel mill in Luleå and Oxelösund (Sweden), and Raahe (Finland).
- SSAB's Raahe plant has two furnaces producing raw iron that is refined into steel at the steel foundry.
- Steel billets are formed using the molten steel, which is rolled into products at the hot rolling mill.









Slag, By-Product

- Slag from the steel making process is poured onto the surface to cool.
- The vanadium has been concentrated in the steel making process. The slag now contains up to 4.4% V₂O₅ (vanadium pentoxide).
- Once the slag has cooled it is • loaded and transported for screening.
- Slag is screened to separate lump which is returned to the blast furnace and fines which are stockpiled.

150 – 200 kg of BOF slag is produced per tonne of steel

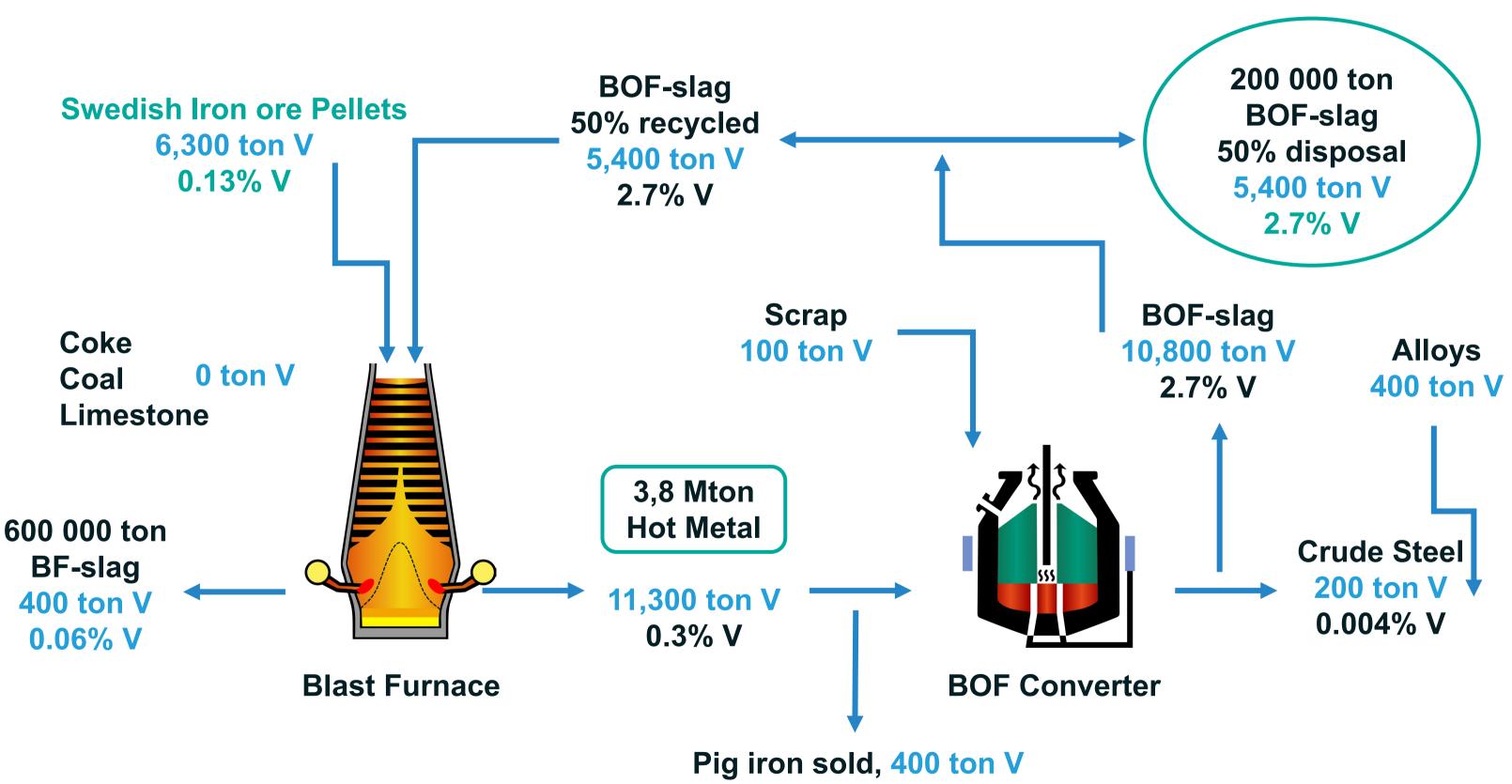


Photo credits: SSAB





High Level Steel Mill Flowsheet and Vanadium Deportment







Location and Stockpiles

SSAB slag stockpiles and production

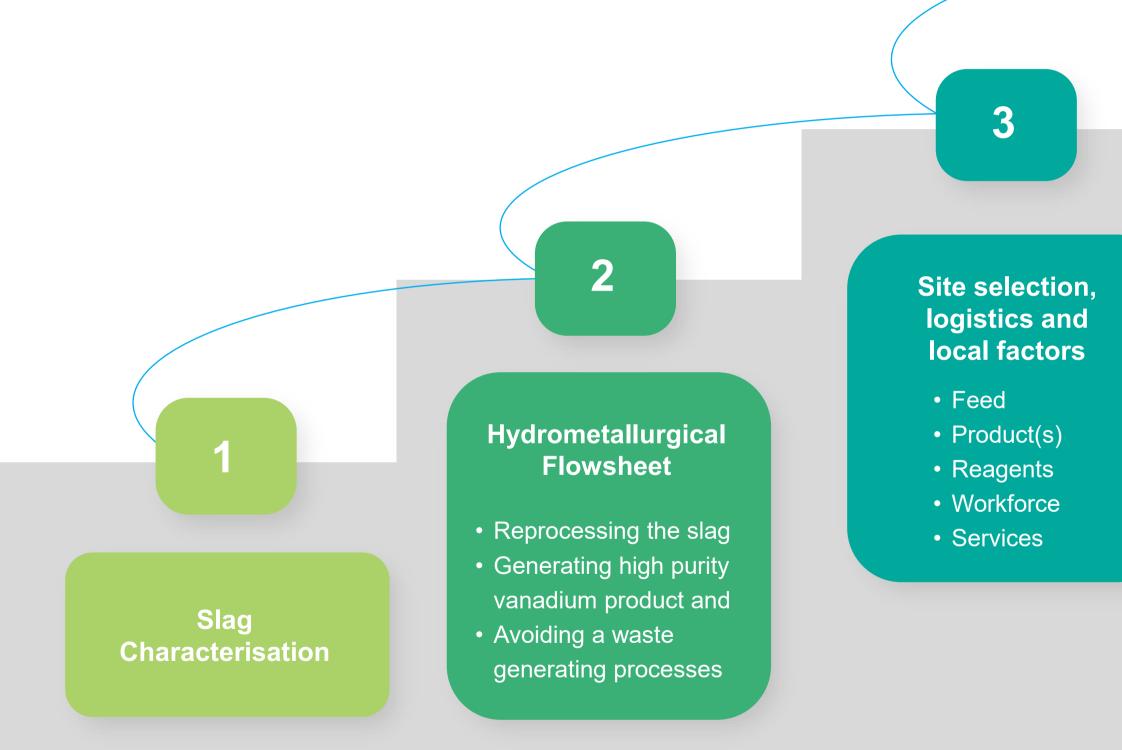
- Planned 300,000 tpa BOF slag feed.
- Potential feed slag already stockpiled and new arisings.
- Several potential suppliers in Europe (e.g. SSAB, Salzgitter, Tata, H2GS etc.) and elsewhere (e.g. CAP).







Project Development





Permitting, environmental

4

Development timeline

5

- Late 2019: Opportunity identification
- Late 2019 to early 2020: Concept testing, bench scale
- Late 2020: Mini-pilot plant (120 hours at 1 kg slag/hour)
- Mid 2021: Full scale pilot plant (total 24 days in 3 campaigns, 25 kg slag/hour)
- Engineering and financing



Vanadium Recovery

Typical of SSAB BOF Slags

Mineralogy of the slag

Table 1: Typical chemical compositions of BOF slag

Radical	Composition range (Wt.%)	Phases
CaO	30 – 50	C_3S , C_2S , [*] CaO, RO
SiO ₂	10 – 15	C_3S , C_2S , other silicates
Al ₂ O ₃	1 – 3	Aluminosilicates,
MgO	5 – 15	Oxides and silicates
MnO	1 – 5	Oxides and silicates
Fe total	10 – 30	Ferrite, FeO, Fe ₂ O ₃
¹ CaO	2 - 10	CaO
P ₂ O ₅	1 – 3	Silicate phases
SO3	0.1 – 0.3	

*CaO-free lime

Calcium silicates: $C_2S = 2CaO.SiO_2$ (Larnite) and $C_3S = 3CaO.SiO_2$ (Hatrurite)



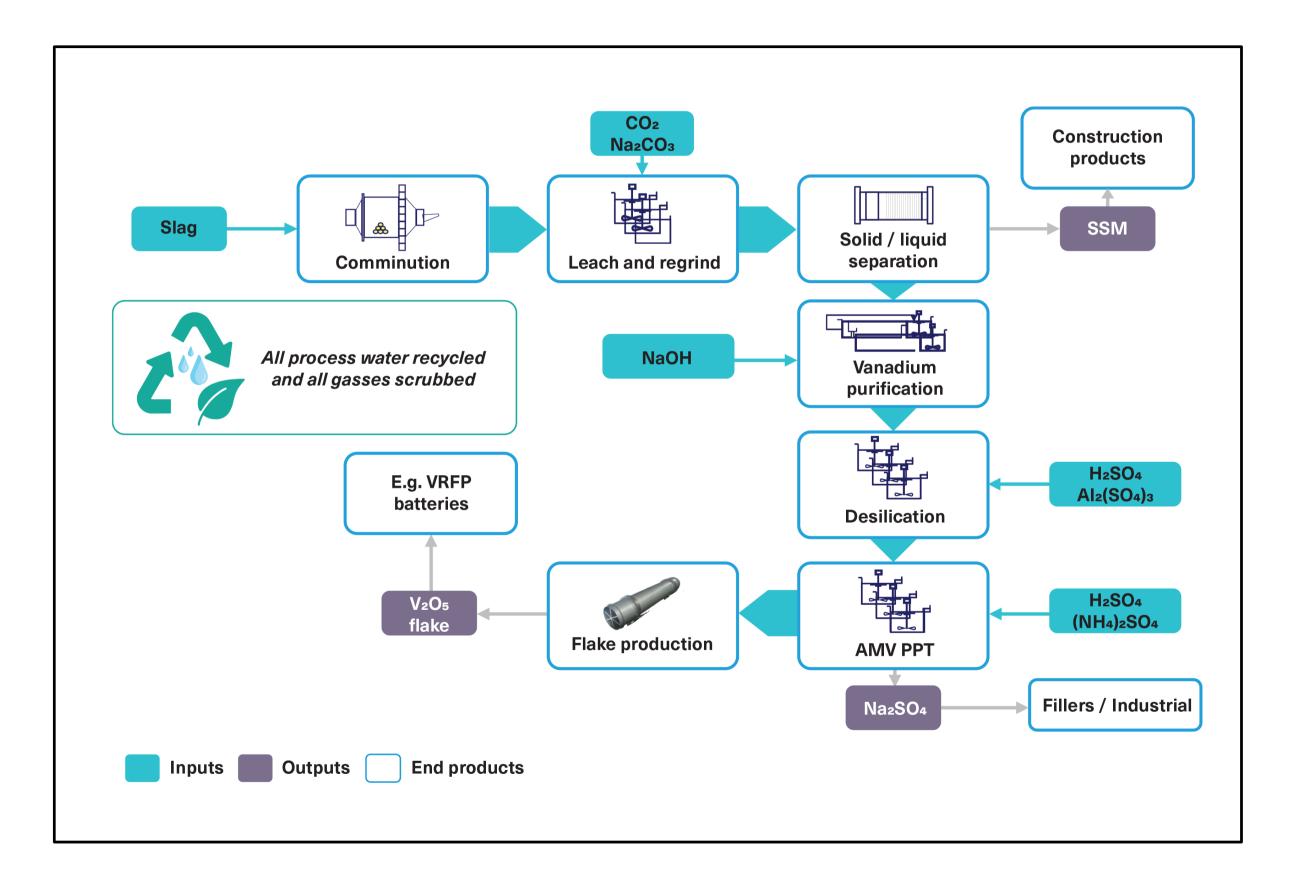
Composition of the slag

Indicative species

Compounds	Percentage (%)
CaO	40 – 50
Fe ₂ O ₃	20 – 25
SiO ₂	10 – 13
V ₂ O ₅	3.0 – 4.5
Mn ₂ O ₃	2.5 - 3.5
Al ₂ O ₃	1.5 – 2.0
MgO	2.0 - 10.0
P ₂ O ₅	0.5 – 1.0
Cr ₂ O ₃	0.2 - 0.6
SO ₃	0.1 – 0.2



High Level Flowsheet – Vanadium Recovery







Process Chemistry 1

Leach process, requires liberation through fine grinding with calcium chemistry the main feature:

Carbonation of calcium minerals and calcite formation

 $Ca^{2+}_{(aq)} + CO_3^{2-}_{(aq)} \rightarrow CaCO_{3(solid)}$ $CaO_{(solid)} + CO_3^{2-}_{(aq)} + H_2O \rightarrow CaCO_{3(solid)} + 2OH^{-}$ $Ca(OH)_{2(solid)} + CO_3^{2-}(aq) \rightarrow CaCO_{3(solid)} + 2OH^{-}$

Carbonate generation •

 $2OH_{(aq)} + CO_{2(qas)} \rightarrow CO_3^{2-}(aq) + H_2O$

- Lixiviant regeneration with CO₂ being the "consumed" reagent and carbon sequestration a byproduct of the • process.
- Calcite precipitation on mineral surfaces leads to multi-stage leaching and regrind requirements.
- pH control for selective leaching and reduced impurities in PLS.
- Leach residue suitable for green concrete applications •





Process Chemistry 2

Purification and concentration by solvent extraction:

- PLS conditioning and fines filtration (Silica removal, prevention of crud)
- Selective solvent extraction and return of the raffinate (NaOH/Na₂CO₃ solution) to the comminution/leach circuit.

Ion exchange of vanadate and hydroxide – long chain quaternary ammonium salt extractant and long chain alcohol phase modifier in an aliphatic diluent.

- Optimisation of the O:A ratios to achieve vanadium concentration into the strip circuit ([V] from ~ 5 g/L in the PLS to ~ 50 g/L in strip).
- **Optimise the V:Na ratio** in the strip to minimise NaOH use and by-product Na₂SO₄.





Process Chemistry 3

Vanadium Product Recovery:

Desilication $[Al_2(SO_4)_3+H_2SO_4]$ followed by standard vanadium recovery steps:

AMV precipitation

 $2VO_{3(aq)} + (NH_4)_2SO_{4(aq)} \rightarrow 2NH_4VO_{3(solid)} + SO_4^{2-}(aq)$

- AMV deammoniation (high temp) $2NH_4VO_{3(solid)} \rightarrow V_2O_{5(solid)} + 2NH_{3(gas)} + H_2O_{(gas)}$
- Ammonia scrubbing ammonium sulphate regeneration
 - + $2NH_{3(gas)}$ + $H_2SO_{4(aq)} \rightarrow (NH_4)_2SO_{4(aq)}$
- Sodium sulphate by-product from AMV barren solution





PFS based on Successful Mini Pilot Plant

- Successful demonstration of flowsheet in a 120-hour, continuous test fed at 1 kg/hr slag
- Exceptional product purity of > 99.5% V_2O_5 ullet
- Vanadium recoveries of around 75 %
- Leach residence times reduced by 50 % ulletfrom Scoping Study design - positive implications for capital costs









Feasibility Study based on Successful Pilot Plant

- Successful demonstration of flowsheet in continuous pilot plant; 3 campaigns, total 24 days of 25 kg/hr continuously fed slag
- Exceptional product purity of > 99.5 % V_2O_5
- Vanadium recoveries of averaged 74 %
- Leach residence times and SX further optimised - positive implications for capital costs
- Lixiviant regeneration and recycle
 demonstrated









Pilot Plant











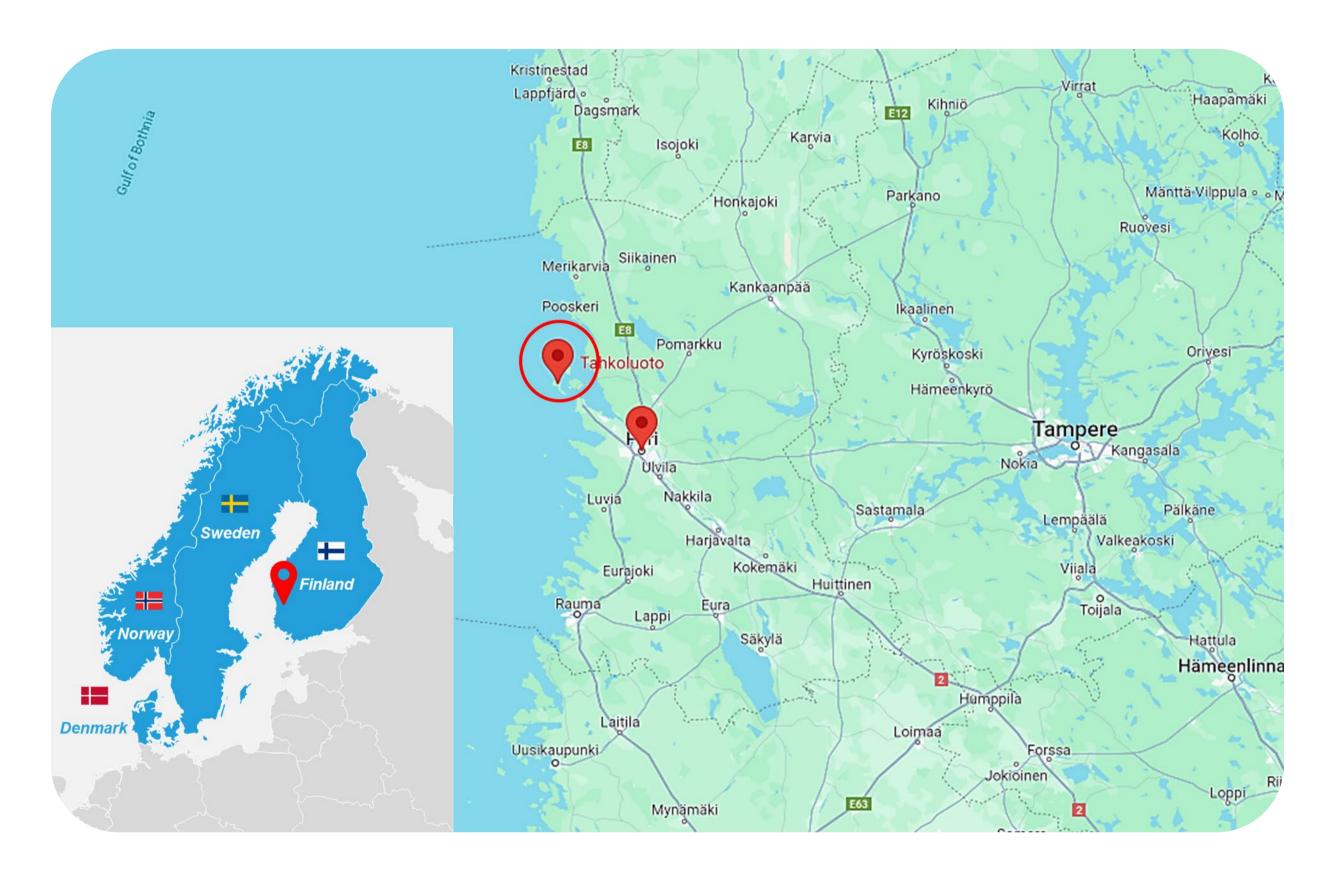








Pori, Finland – Tahkoluoto Port







Site Location – Tahkoluoto







Pori, Finland – Proposed first Vanadium Recovery Plant

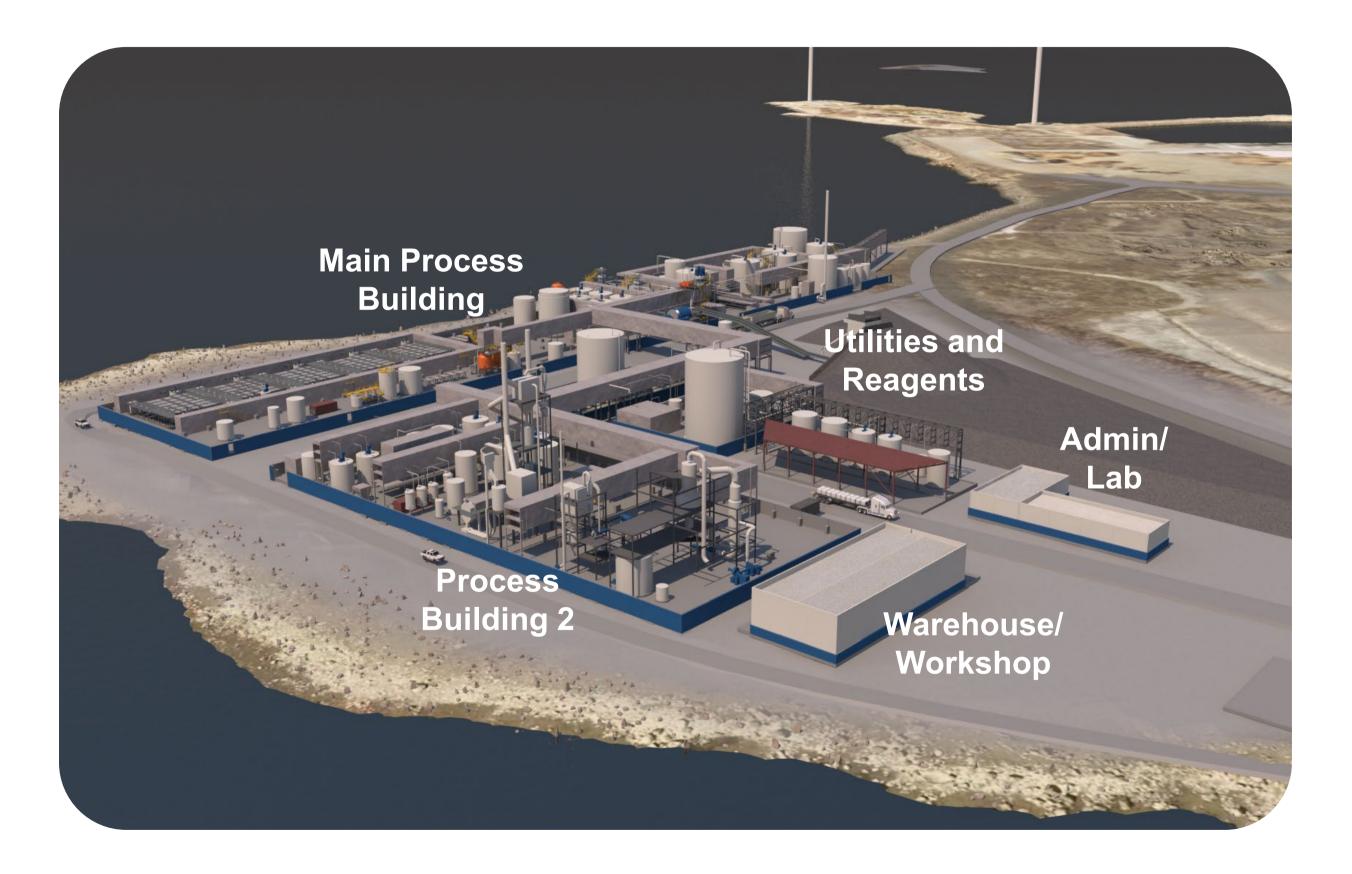
- City of 86,000 inhabitants with a long history as a hydrometallurgical center of excellence
- Access to a 'build-ready' 20 hectare industrial-zoned site adjacent to the deep water, year-round port with rail access to the bulk import/export and chemical berths
- Access to renewable power and other utilities and free access to its industrial sources of CO₂ for capture and sequestration in Neometals' proprietary process flowsheet







Process Building Layout

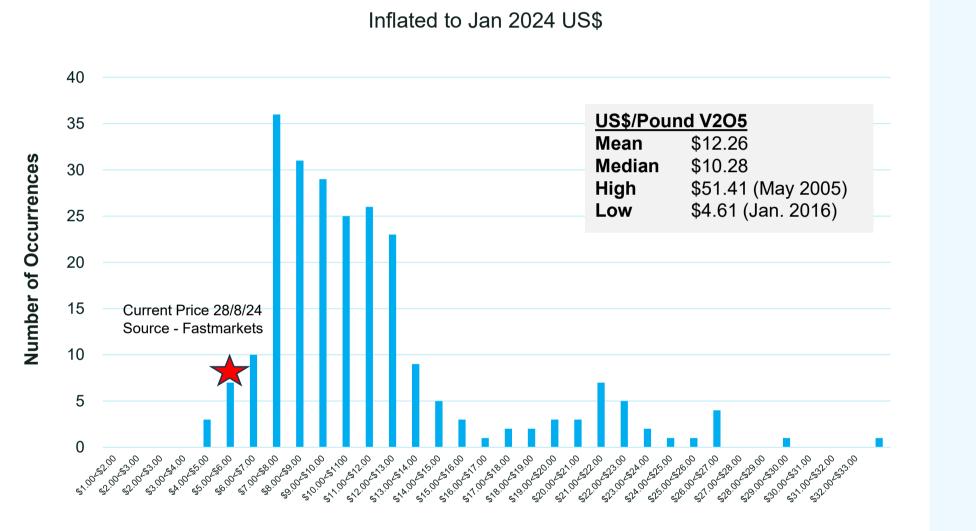






Lowest Quartile Cost Position

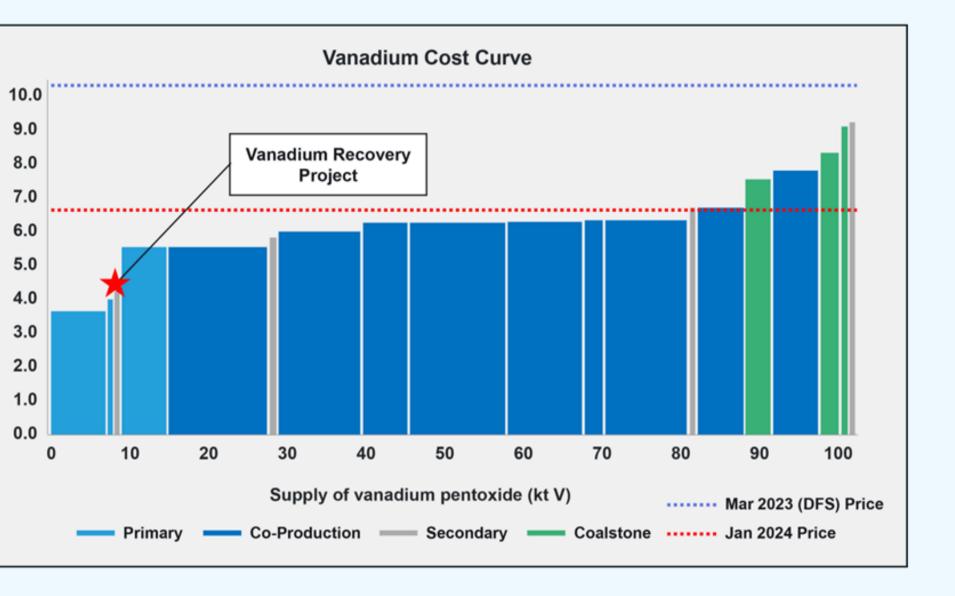
V₂O₅ Real Price Distribution Chart Jan. 2004 - June 2024



Source Metals Bulletin publication, TTP Squared Inc. and Fastmarkets

For further information, refer to ASX release dated 8th March 2023 – Vanadium Recovery Project Delivers Strong Feasibility Results





Production cost (US\$/Ib)



Vanadium Recovery

VRP meets many of the goals of Circular Hydrometallurgy

- Recovery of values from by-product slag
- Reagent regeneration and re-use
- Zero solids waste discharge lacksquare
- Minimal liquid/gas discharge
- Use of green electricity
- Overall process produces carbon negative vanadium

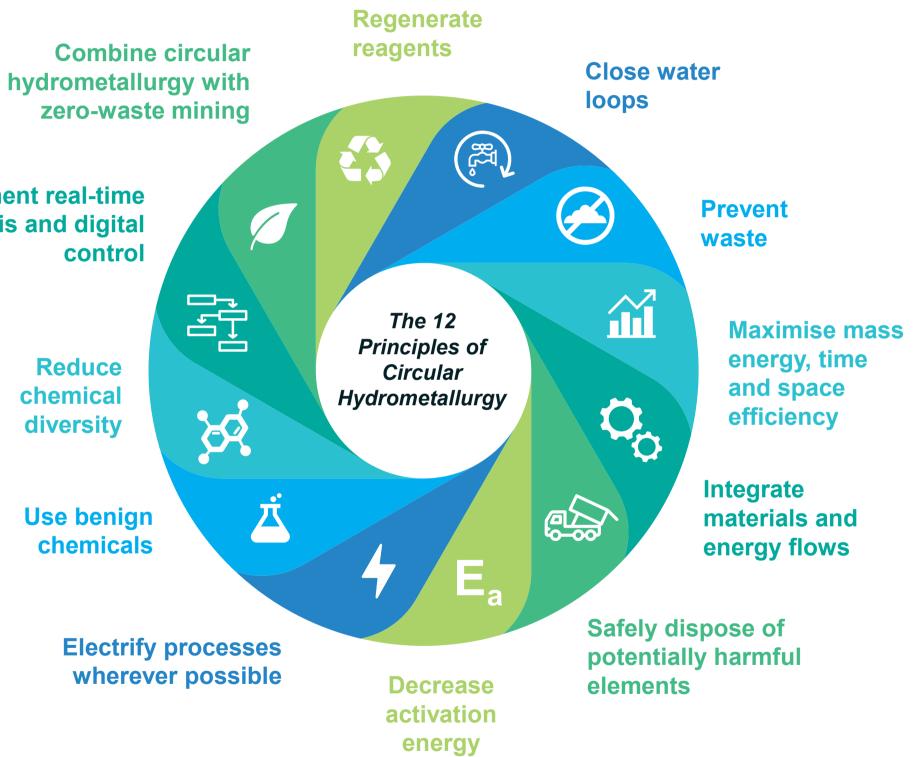
Implement real-time analysis and digital

> Reduce chemical diversity

Use benign chemicals







Source: Tom Jones, The Twelve Principles of Circular Hydrometallurgy, Journal of Sustainable Metallurgy 9 (1) (2023) 1-25.



Sustainability – CO₂

Processing slag waste material to recover valuable vanadium

Life Cycle Analysis ulletcompleted by Minviro (UK) as part of our studies 15 Average CO_2 emissions for • Kg CO₂ eq per kg V₂O₅ V_2O_5 production is negative 5 4 - 5 kg per kg of V₂O₅ equivalent 0 -5



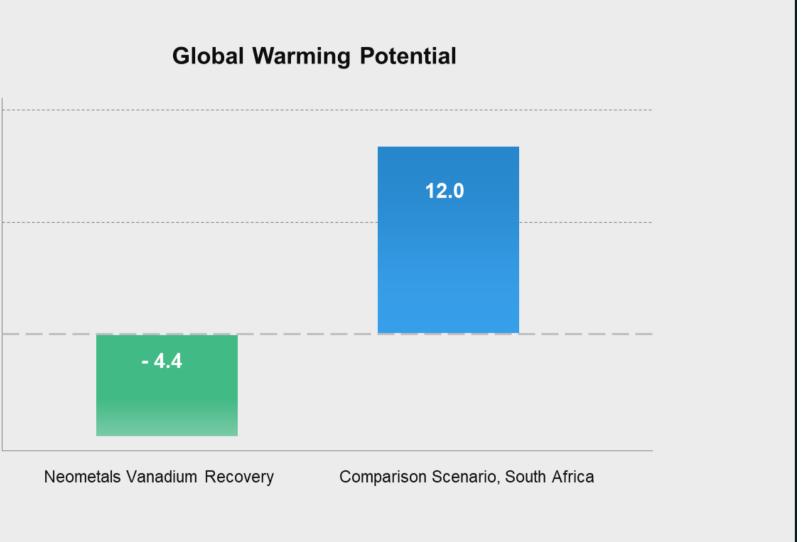


Figure: Comparison of global warming potential impact for producing V₂O₅ at Pori Finland compared to South Africa





Thank you

I'm happy to answer questions now or email me at:

drobinson@neometals.com.au

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Vanadium Recovery Project

Pilot Plant (June 2021)

- **Process:**
 - Three separate campaigns, operating over 24 days (24 hour, 2-shift operation), one each focused on Luleå, Raahe and Oxelösund slag
- Feed at 25 kg per hour
- **Process:**
 - Crushed slag delivered (< 3 mm)
 - Ball Milled in process water to reduce particle size
 - Leach feed at selected pulp density and Na₂CO₃ concentration
 - 3 stages of leaching with two-interstage regrind mills warmed and held at selected pH with CO₂ sparging
 - Leach discharge washed on the filter and discharged to a repulp wash circuit
 - PLS prepared by further pH adjustment and filtration for Solvent Extraction
 - Vanadium strip solution taken through conventional steps of;
 - Desilication
 - Ammonium metavanadate precipitation, filtration and washing
 - Deammoniation to form vanadium pentoxide (V_2O_5)
- July 25th completed 24 days (24 x 7) of pilot plant operation at 25 kg slag feed per hour.

